

SOFC Development Update at FuelCell Energy



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18th Annual Solid Oxide Fuel Cell (SOFC) Project Review Meeting
Pittsburgh, PA

June 12-14, 2017

■ Introduction

- Project Objectives
- FCE's SOFC Development and Deployment Pathway

■ Progress in SOFC Technology

- Cell Technology Development
- Cell and Stack Manufacturing
- Transformational Technologies for Breakthrough Cost Reduction

■ System Development and Testing

- 200 kW System Development and Testing
- 100 kW Modular Power Block (MPB) Development
- MW-class Module Concept
- Related System Applications

■ Summary

Develop SOFC technology suitable for ultra-efficient central power generation systems (coal and natural gas fuels) featuring $\geq 97\%$ CO₂ capture with significantly lower costs ($\geq 20\%$ lower) than Baseline approaches



Conduct cell & stack R&D focusing on performance, reliability, cost and manufacturing enhancements



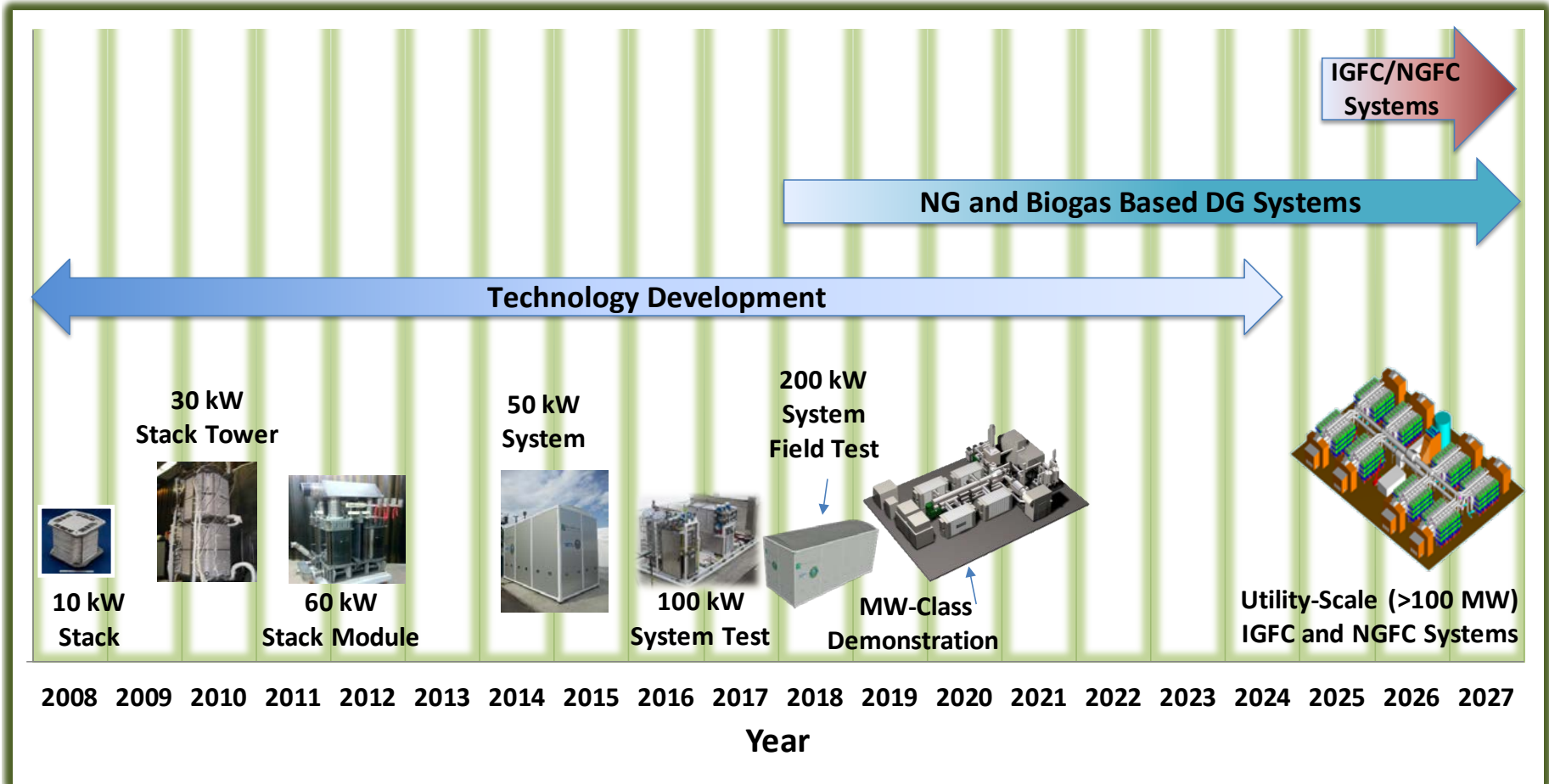
Develop Innovative SOFC cell and stack technologies with the potential for transformational performance and cost characteristics



Design, build and operate 100-200 kW demonstration systems using natural gas fuel to validate stack operation in the field



Develop concept system design and stack module for a MW-class power plant, and estimate stack costs



- Ongoing technology development and system field testing is laying the foundation for cost-competitive DG and centralized SOFC power systems

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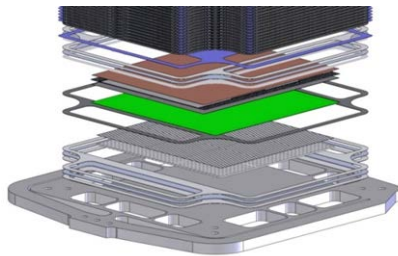
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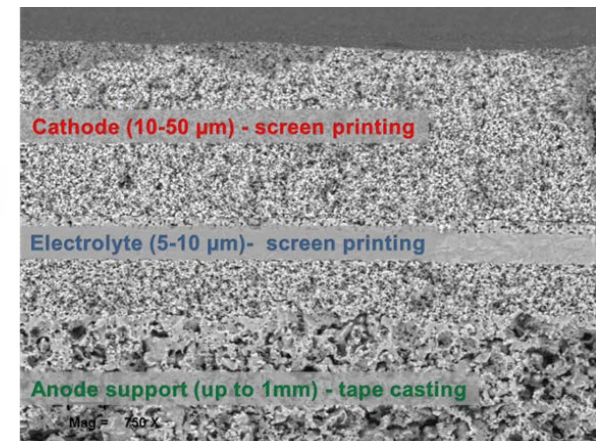
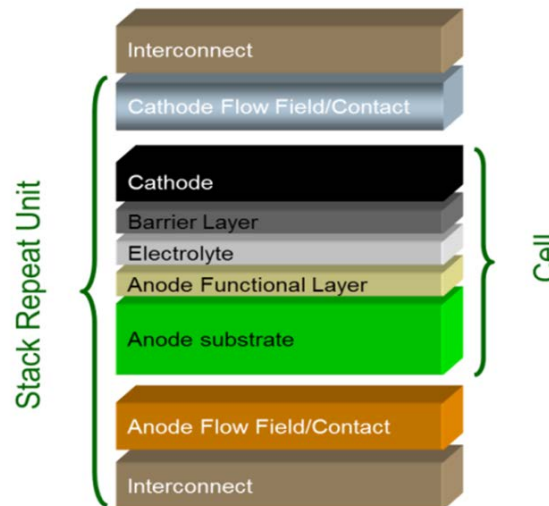
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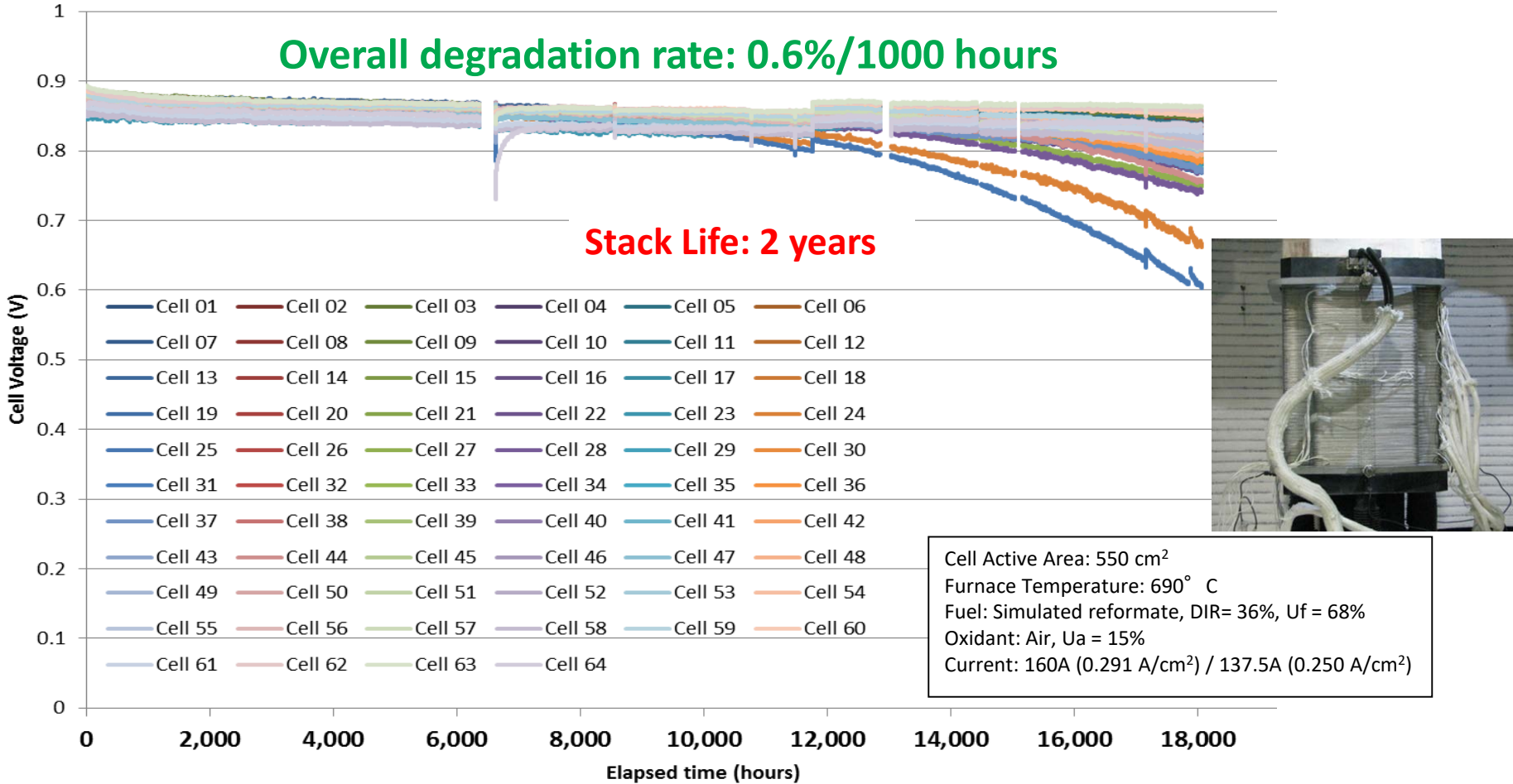
■ Summary



- Cell:
 - Planar anode supported
 - 0.6 X 250 X 250 mm with 550 cm² active area
 - Manufactured by tape casting, screen printing and co-sintering
- Stack
 - Ferritic stainless steel sheet Interconnect
 - Compressive ceramic seal
 - Integrated manifolding with formed flow field layers
 - 120 Cells in a standard stack with 16 kW output @ 160 A

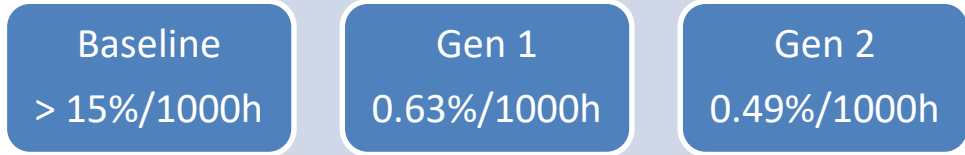


64 cell Large Area Stack Testing with Cr Tolerant Technology Gen 1.0

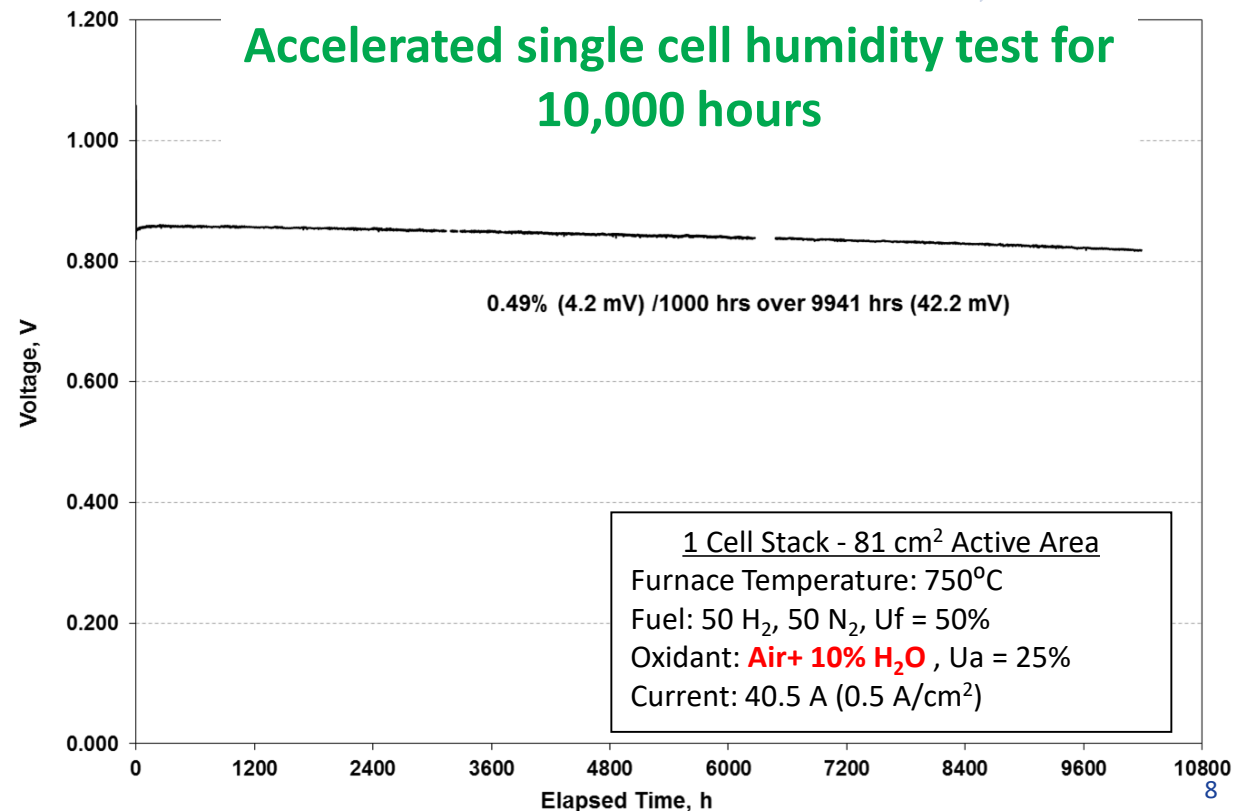


Identified Issues	Improvement
Inadequate contact	Contact paste and contact / seal balance optimization
Cr poisoning	Cr tolerant technology development
Manufacturing Reliability	Gage R&R, production and QC tooling improvement

- Improve coating coverage
- Ce doped Co-coated IC
- Gen 2.0 Cr Getter

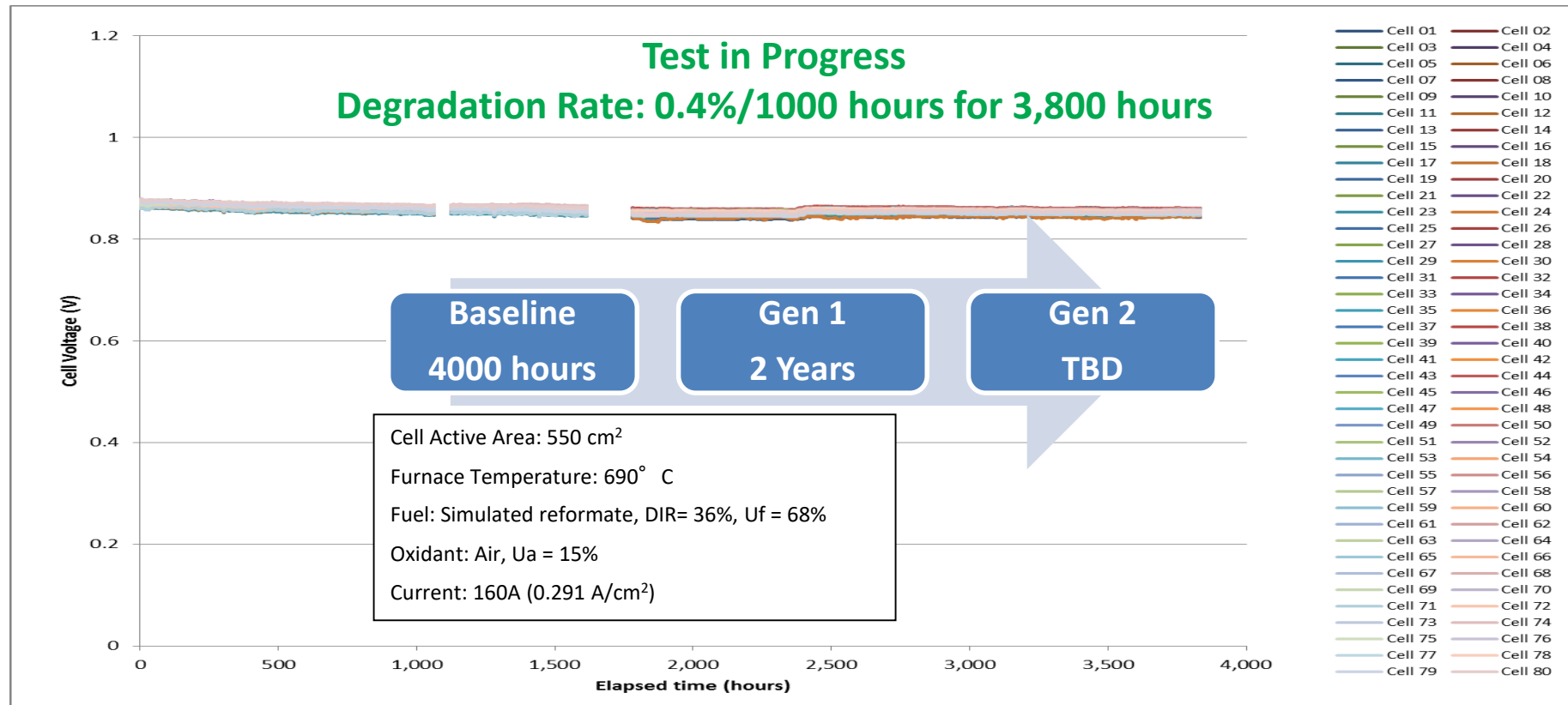


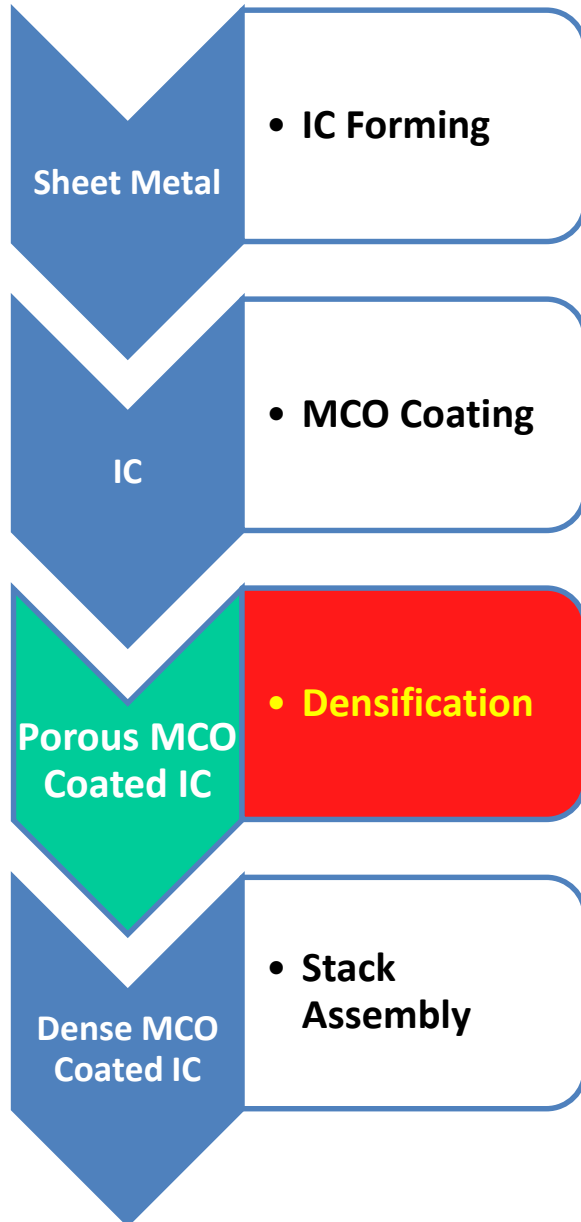
- Gen 2.0 Cr Getter development was focused on improving stability and compatibility of the Cr Getter
- Unique fabrication process was developed to make on-cell Cr Getter stable
- Optimized Cr Getter composition and design were down selected as Gen 2.0 Cr Getter technology for stack



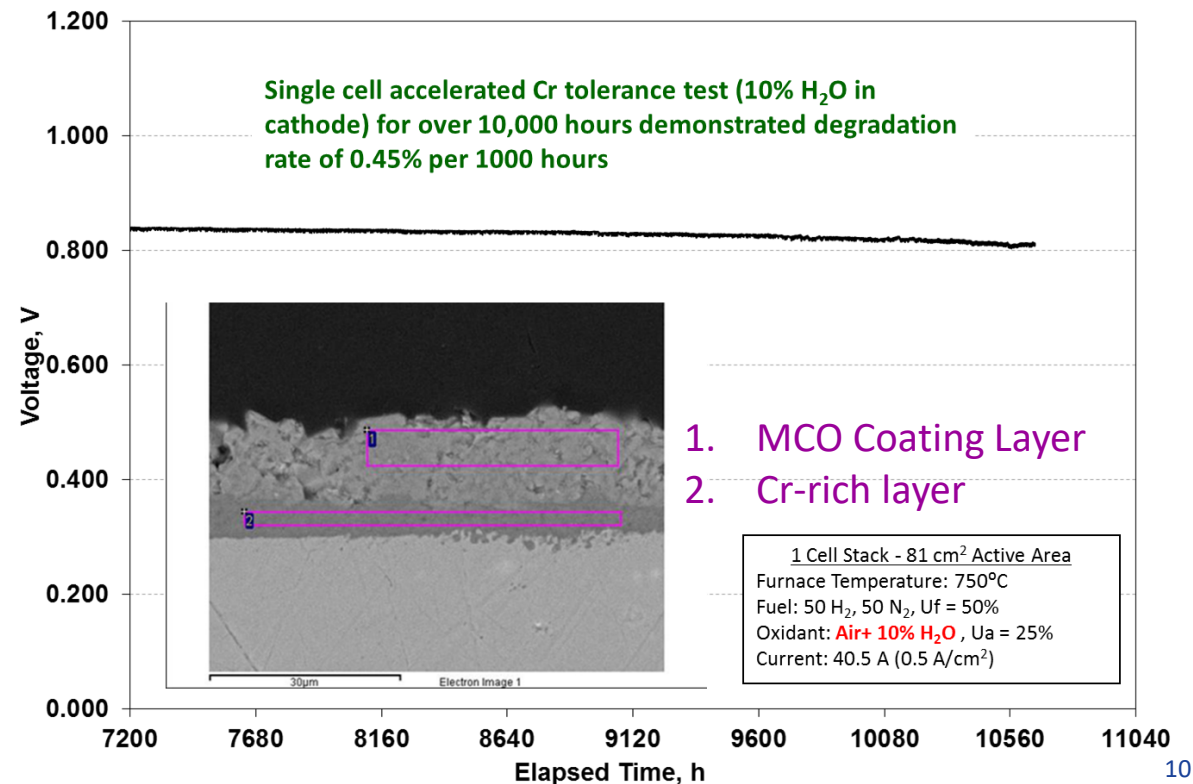
Validation Test: 80-Cell Large Area Stack with Gen 2 Cr Tolerant Technology

Identified Issues	Improvement	Results
Inadequate contact	Contact paste and contact / seal balance optimization	Less than 20 mV voltage spread after 3800 hours of stack operation
Cr poisoning	Cr tolerant technology development	Gen 2 Cr tolerant technology is under evaluation with a 80-cell stack. So far the degradation rate is 0.4% per 1000 hour
Manufacturing Reliability	Gage R&R, production and QC tooling improvement	Incorporated in the cell/stack manufacturing for ongoing production and future deliverable stacks

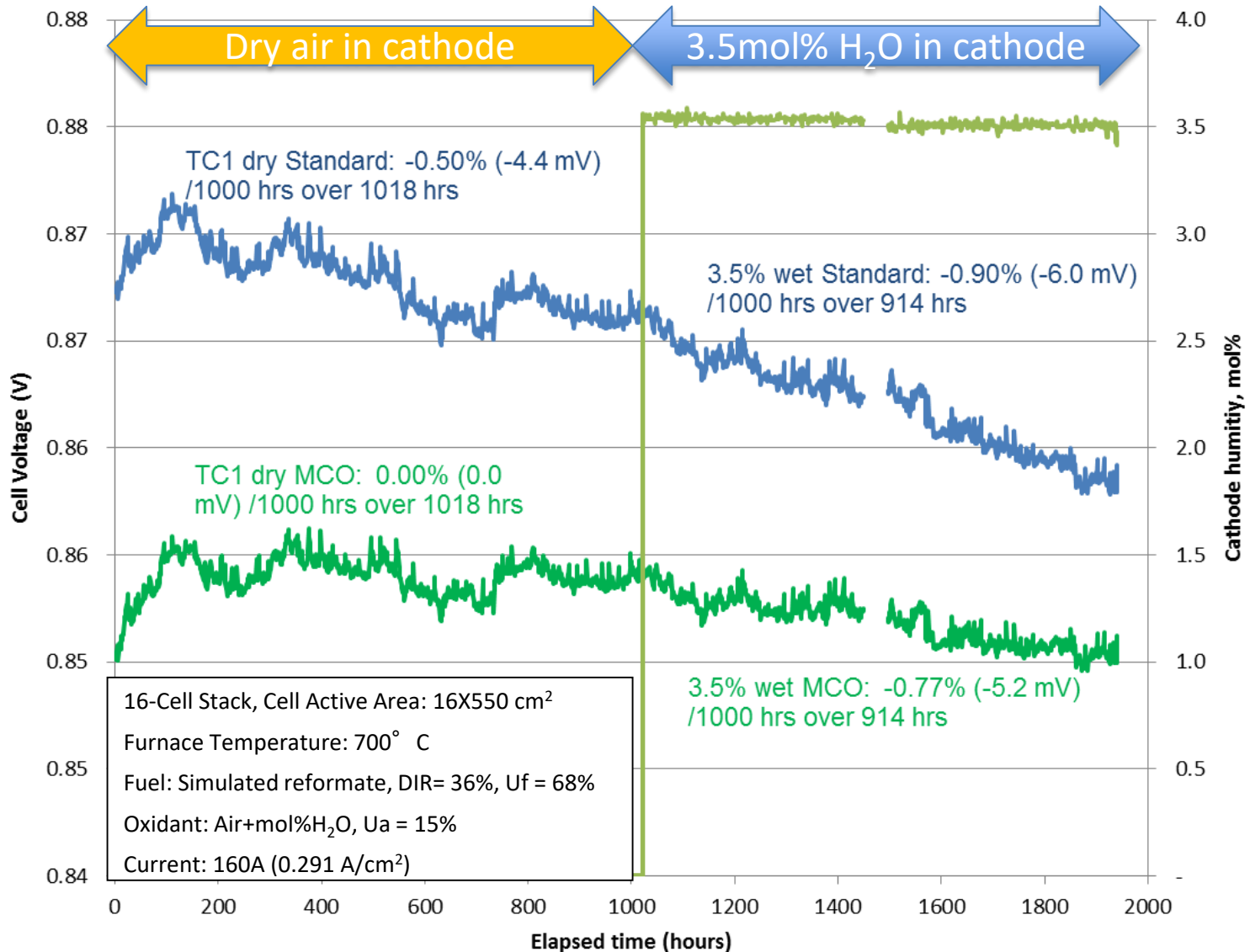




- Issues with ex-situ MCO coating
 - High-temperature (>800 °C) reducing atmosphere densification process leads to high cost and oxides forming at anode side IC
- FCE MCO coating focus on simpler densification process at lower temperature
- Various sintering aids were added to MCO coating

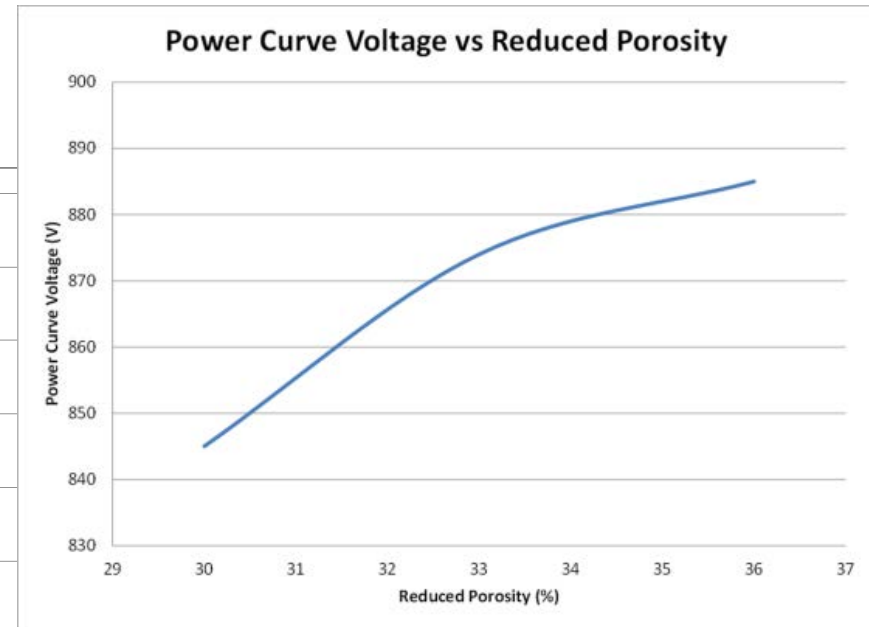
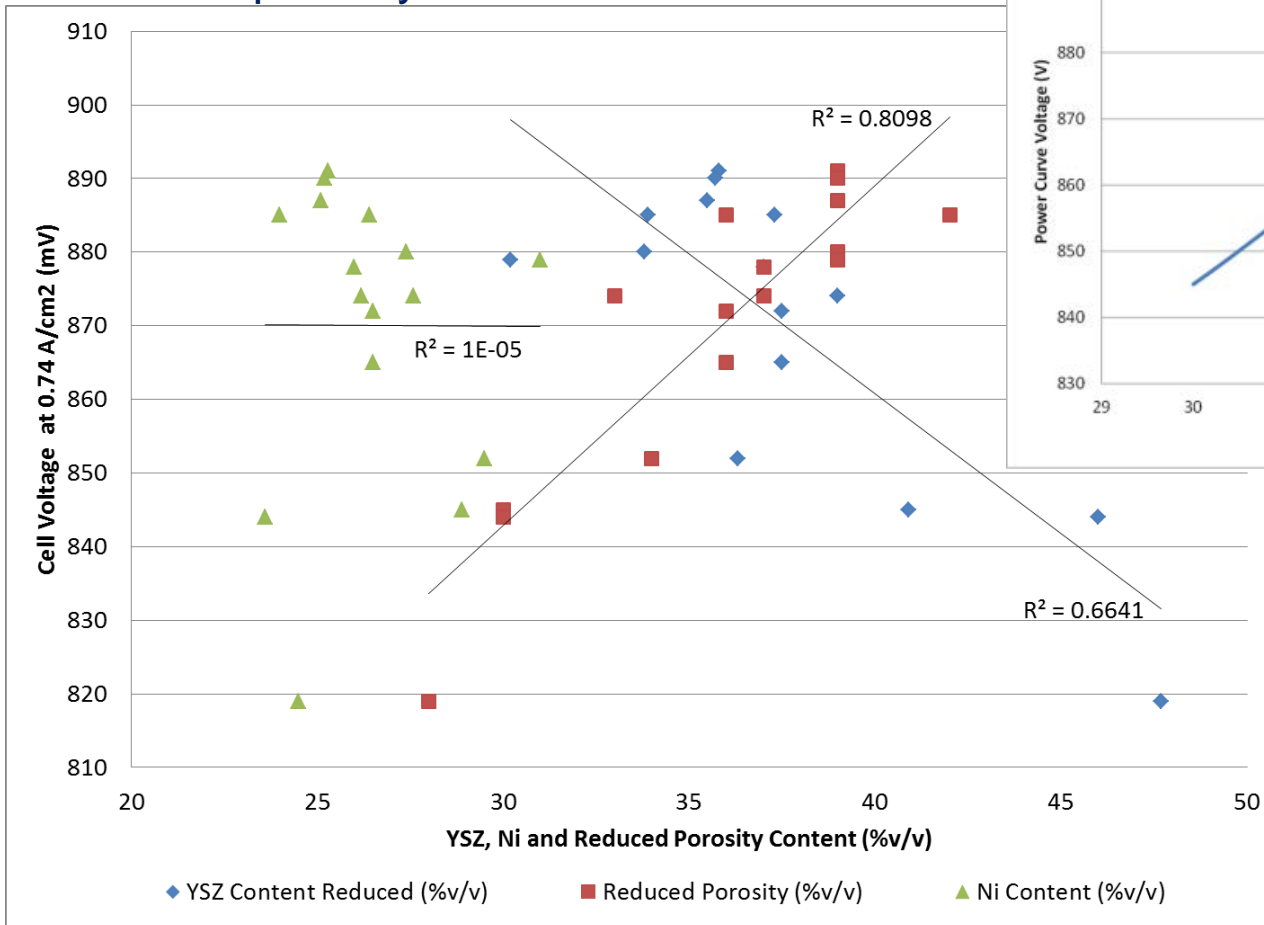


16-Cell Parametric Stack Testing (In Progress) Standard Co-Coating vs. MCO Coating



Cell performance has:

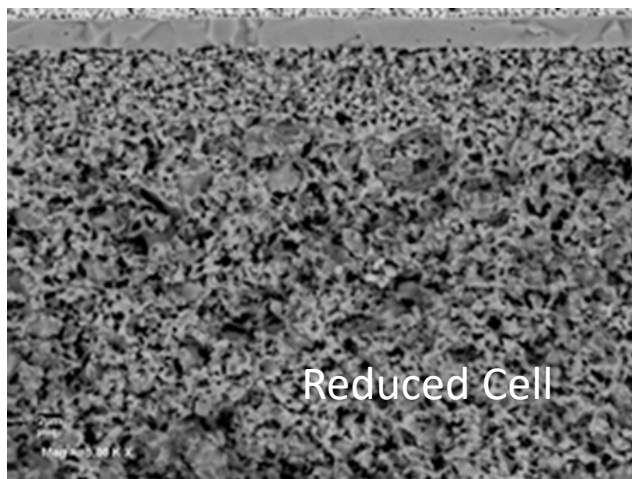
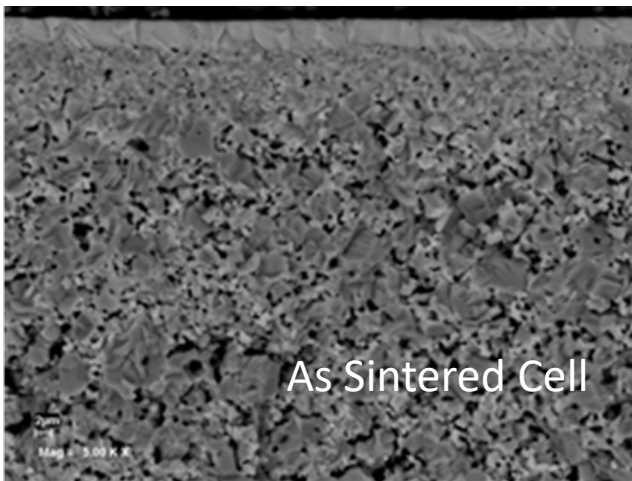
- Strong and positive correlation with anode porosity



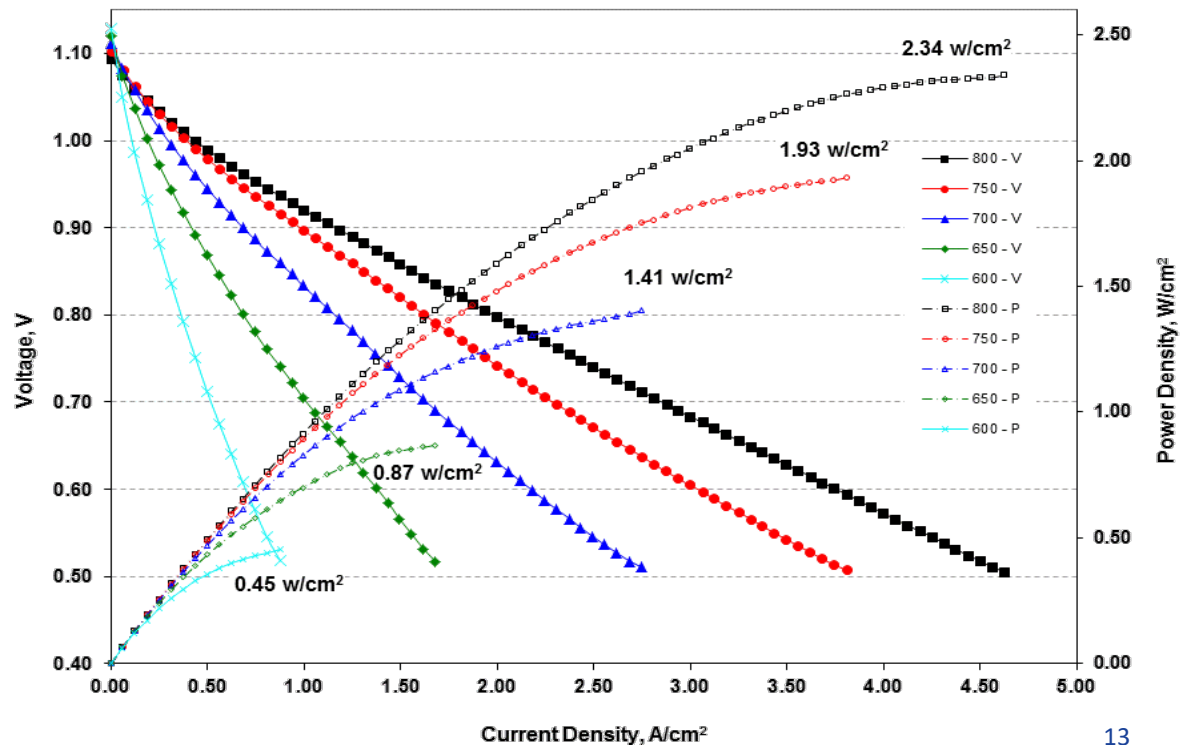
Cell performance has

- Weak and negative correlation with YSZ volume
- No correlation with Ni volume

- The performance of cell at higher fuel utilization of over 80% is affected strongly by anode thickness
- Thin cell with 300 μm anode has the potential to operate beyond 85% fuel utilization



Recent anode development has further improved cell performance (2.34 W/cm^2 at 4.7 A/cm^2)



Objective:

Reduce thickness and increase density of the GDC barrier layer utilizing advanced manufacturing techniques to reduce cost and improve performance

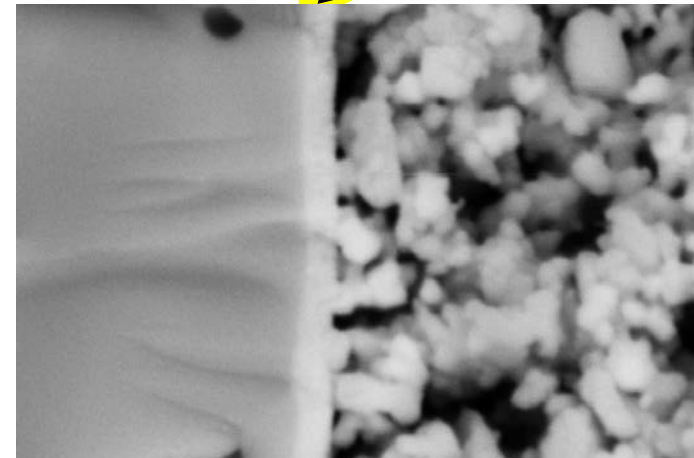
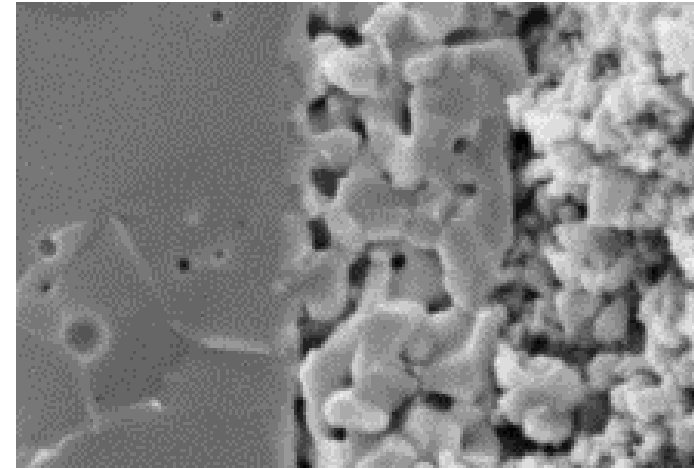
Innovative Solutions Being Explored:

1. Atomic Layer Deposition (ALD) to form a very thin (tens of nanometer) and fully dense barrier layer

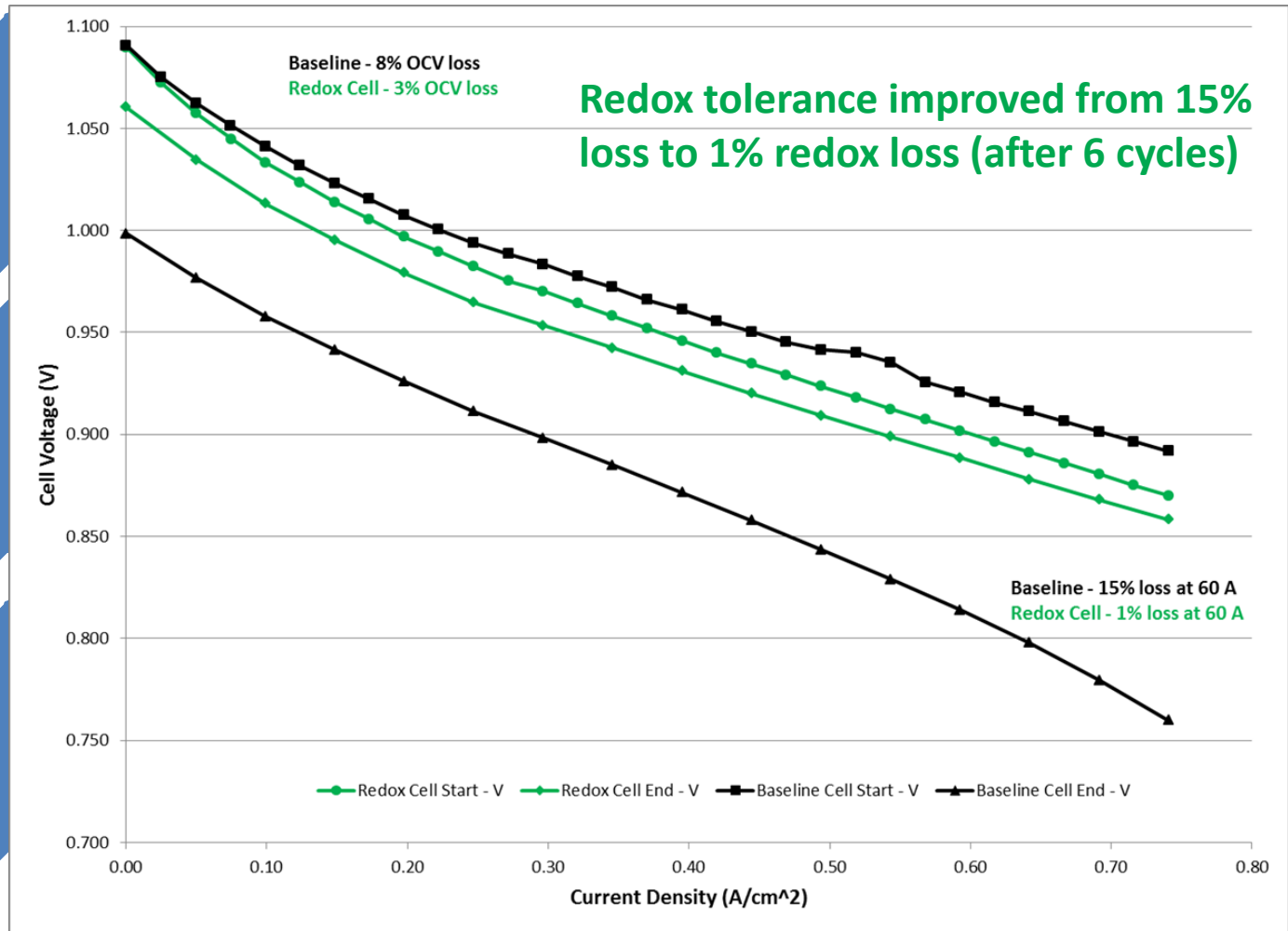
- ALD is commercially used in a wide variety of applications, including ZrO₂ films for DRAM capacitors and barrier coatings for displays
- ALD can be scaled up cost effectively (large batch processing)

2. Reactive Spray Deposition Technology (RSDT) for cost-effective manufacturing of dual-layer GDC barrier layer and cathode electrode on sintered half-cells

- RSDT is a low cost, rapid processing method that can be performed in one continuous process without the need for long sintering times at elevated temperatures
- Deposition is highly customizable (manipulation of process parameters), thereby allowing a single process to deposit a dense or a porous layer



Implementing multi-prong approaches in developing innovative redox tolerant anode-supported cell through reducing anode strain upon Ni re-oxidation



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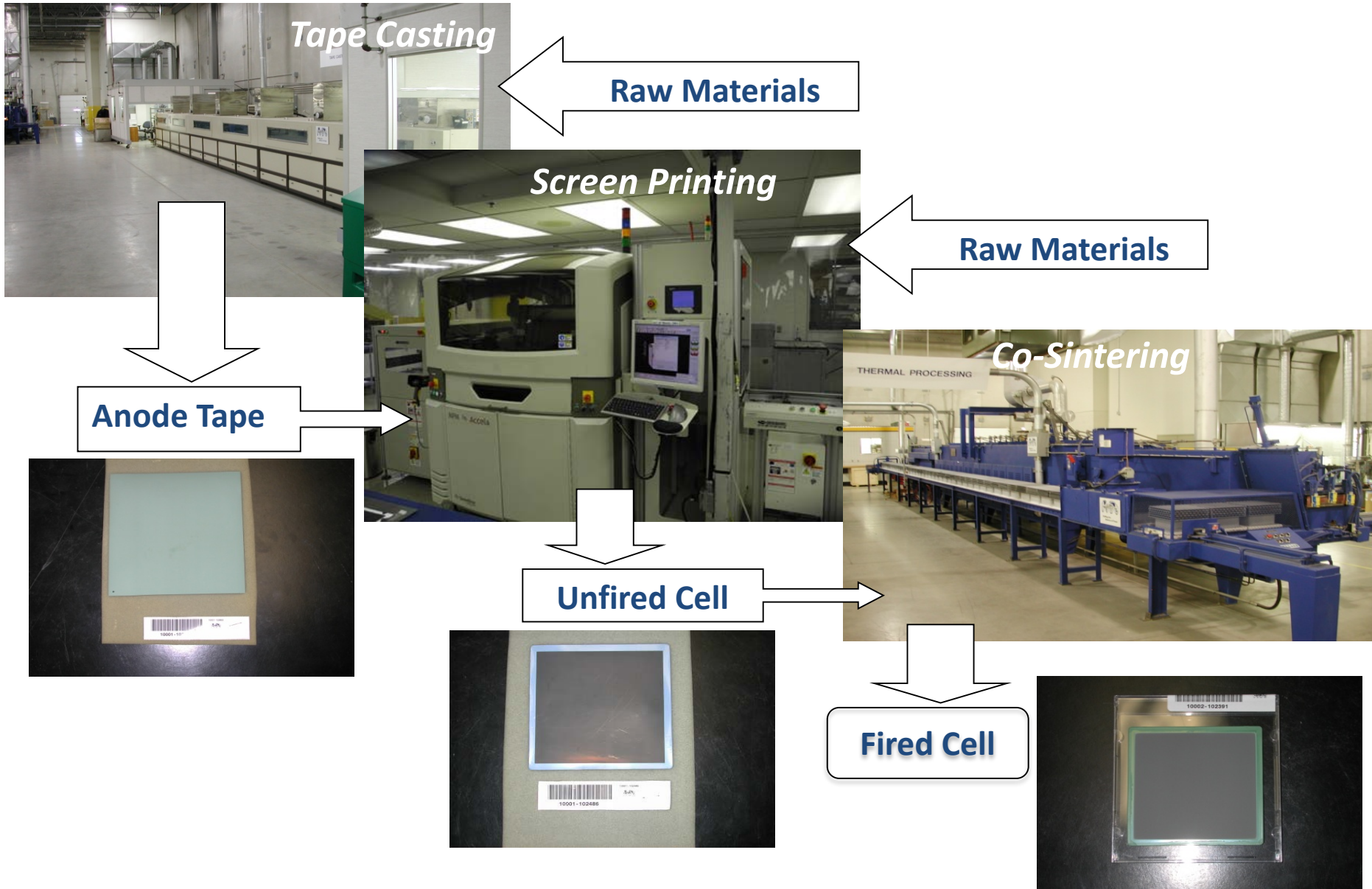
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CELL MANUFACTURING

1. Powder & Paste
2. Half Cell Production
3. Cell Completion

SEAL MANUFACTURING

METALLICS MANUFACTURING

1. Anode and Cathode Flow Fields
2. Spot welding
3. Component kitting
4. Sub-assembly manufacturing

Every Stack is Individually Conditioned and Undergoes Rigorous Factory Acceptance Tests

STACK
ASSEMBLY

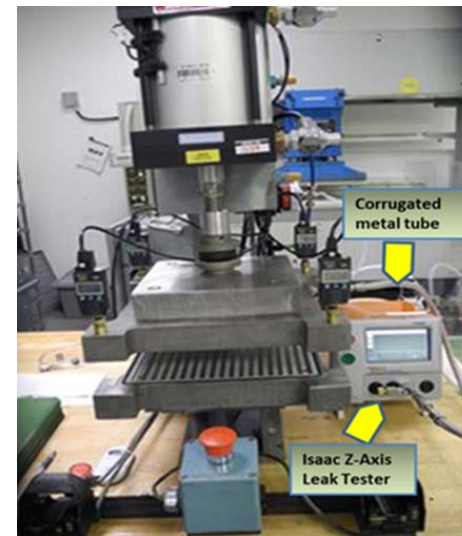
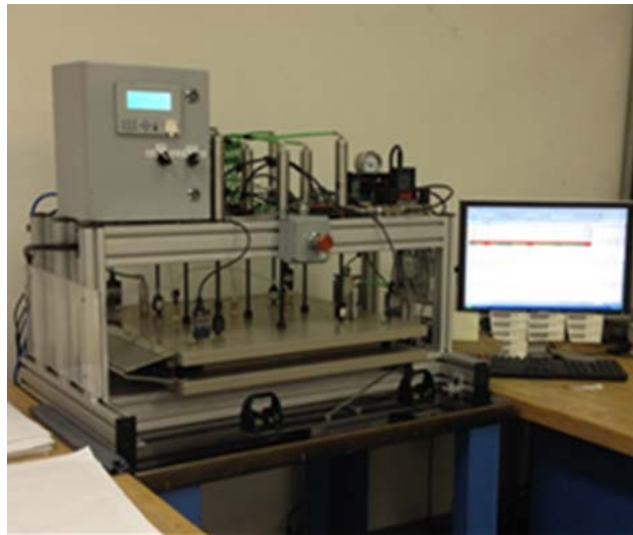
CONDITIONING
& ACCEPTANCE
TESTING

STACKS FOR
MODULE



25kW Test Stands for Factory Acceptance Testing

- Individual stack performance is limited by weakest unit cell, so high reliability is required
- New cell thickness + leak test QC station implemented simulating thickness when compressed in stack with Total Gage Reproducibility and Repeatability (Gage R&R) of 6% (desired target < 30%) with 0.04 mm total tolerance

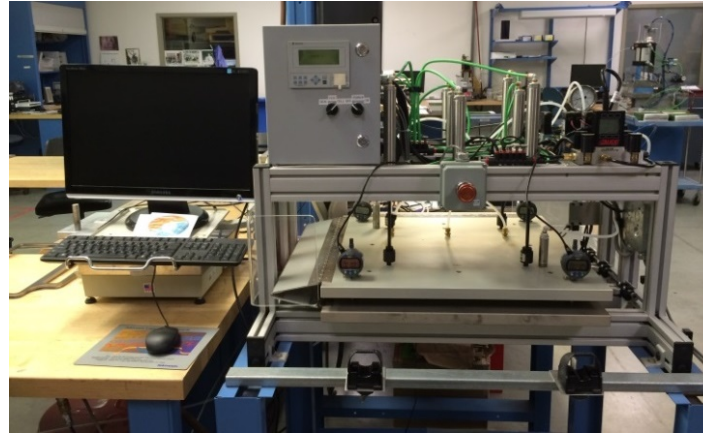


New High-Throughput & Combined
Function QC Stations Ensure
Quality Cell Components



Metallic Part QC Station

*For smaller footprint contact /
flow field materials*



Double Hinge QC Station

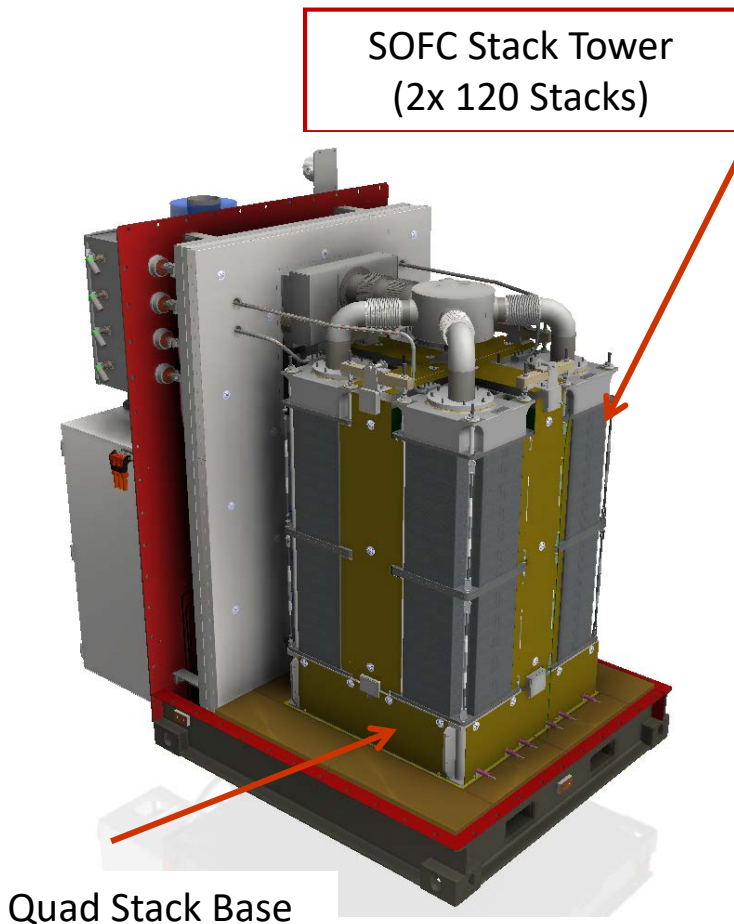
*For full footprint interconnect
and shims*



Flow Field QC Station

For anode flow field screening

- Increased Production Quality
- Reduced Inspection Labor Time
- Increased Stack Operational Reliability



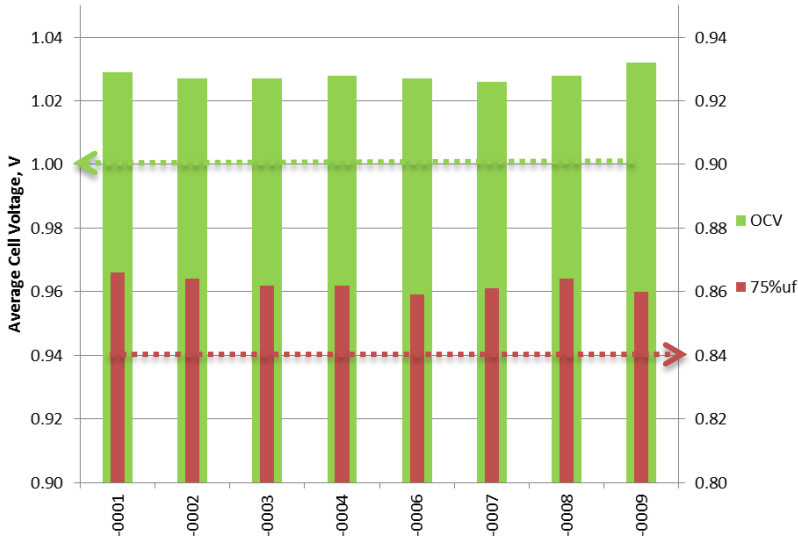
**Each 100 kW Stack Module includes
8 x 120-cell stacks (or 960-cells)**

Module 1 (100-01) (100 kW)	Module 2 (100-02) (100 kW)
GT059879-0001	GT060322-0001
GT059879-0002	GT060322-0002
GT059879-0003	GT060322-0003
GT059879-0004	GT060322-0004
GT059879-0005	GT060322-0005
GT059879-0006	GT060322-0006
GT059879-0007	GT060322-0007
GT059879-0008	GT060322-0008
GT059879-0009	

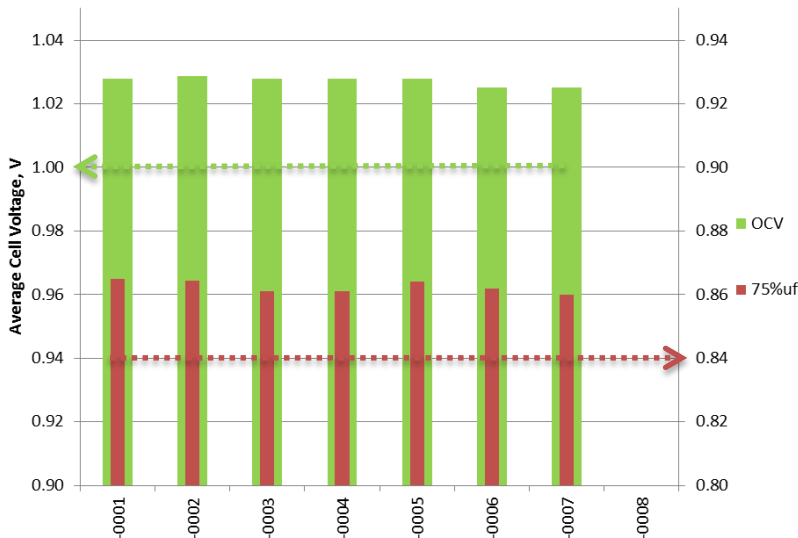
- **200 kW SOFC System: 15/16 = 94% complete (and 94% yield)**

*GT059879-0005 lost due to error in the stack assembly
(One anode flow field was placed in reverse)

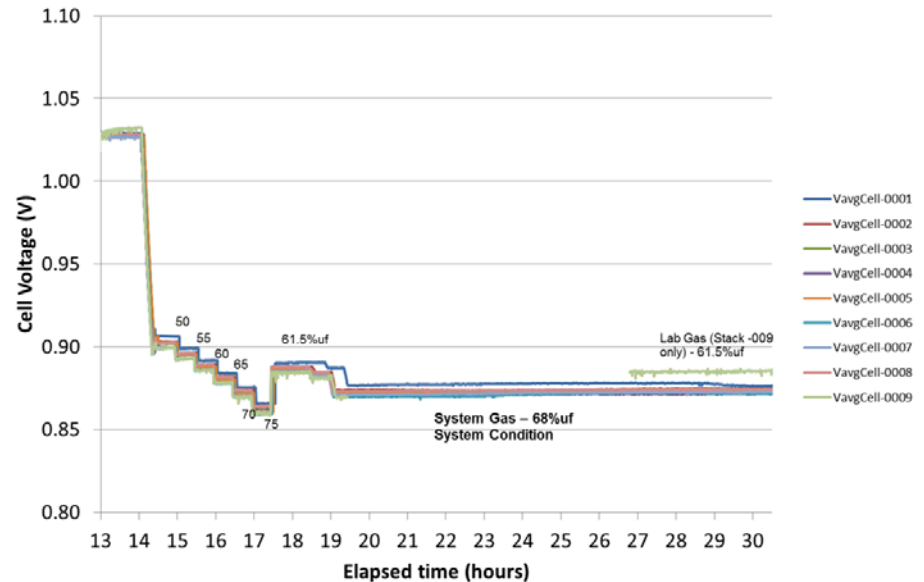
Module 1 Stack Performance



Module 2 Stack Performance

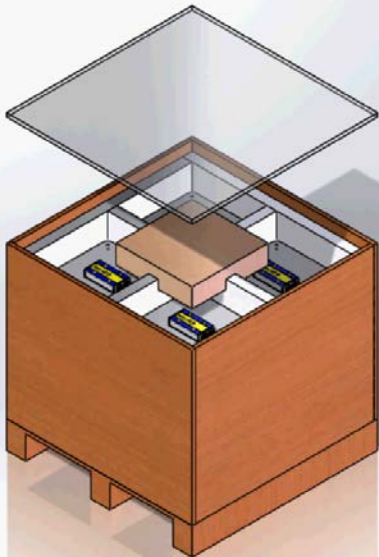
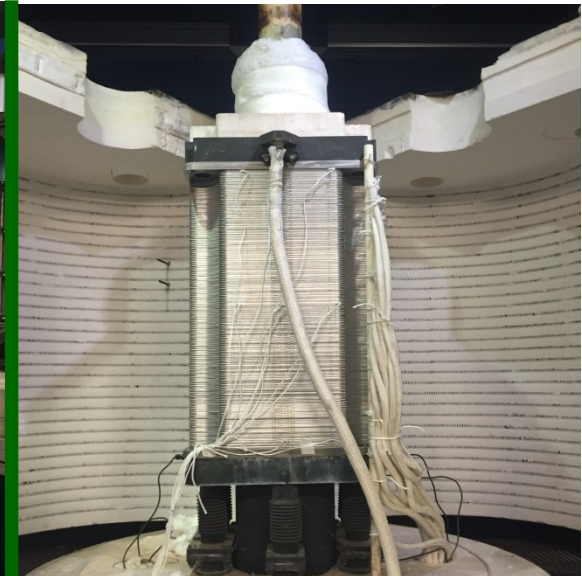
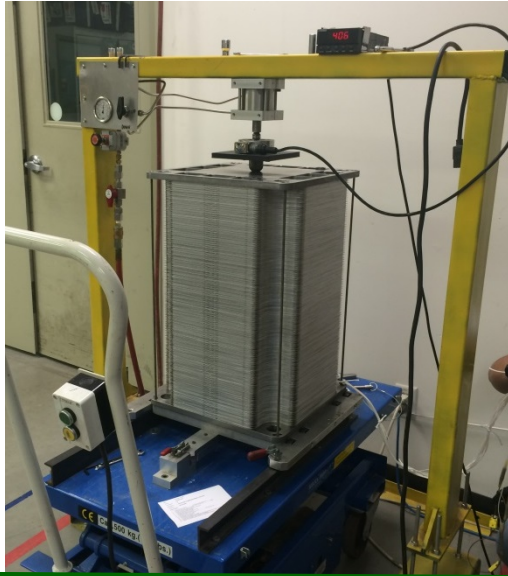


GT059879-0001 to 0009 TCO Average Cell Voltages 120 cell, 550cm² Module 1 400kW, TS29, 27



- **Excellent stack to stack performance reproducibility at high fuel utilization**
 - **0.8% difference (or +/- 0.4%) in average stack voltage**
 - **7 mV standard deviation in individual cell voltages**
- **Stacks for Module 1 + 2 meet cell voltage criteria**

Stacks Built Will be Shipped to Danbury Facility for Module Integration



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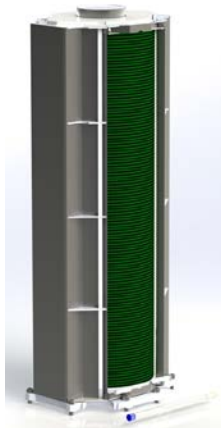
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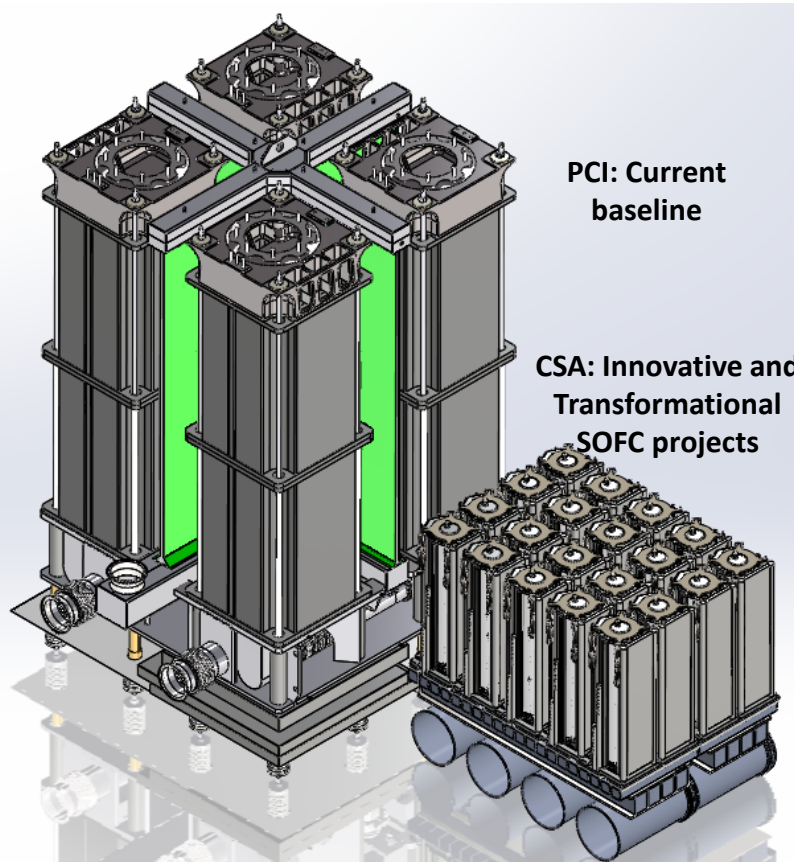
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Current Pre-Commercial Integrated Manifold (PCI) Stack



Compact SOFC Architecture (CSA) Stack with ~10-fold Increase in W/kg Power Density



PCI: Current baseline

CSA: Innovative and Transformational SOFC projects

Comparison of 100 kW Stack Modules

Objective

Develop an innovative stack design enabling significant (> 50%) reduction in stack cost relative to baseline stack design (PCI)

Approach

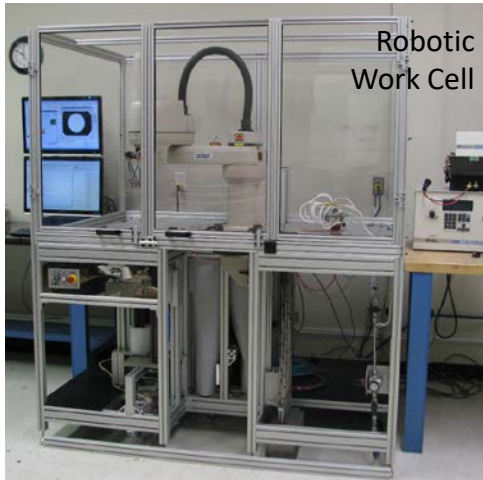
Target significant savings in both cell and stack materials and production labor

Design Philosophy

- Thinned cell and stack components to reduce material content without impacting performance
- Stack design choices that simplify assembly steps and reduce unit cell part counts
- Increased cell count per stack (>300 cells)
- Use of same cell, interconnect and coating materials validated in the large area stack (PCI) platform

Manufacturing Approach

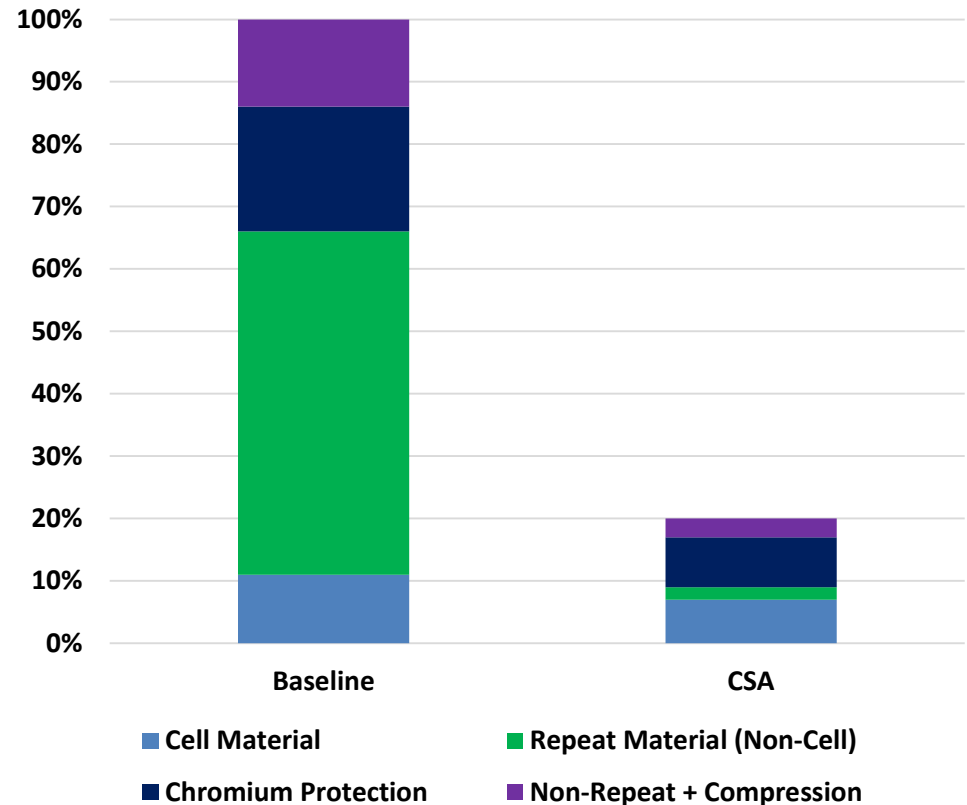
- Design for advanced high-throughput manufacturing technologies for thin components taking cues from CD / DVD manufacture
- Utilize high speed pick and place robot (Adept i600) for efficient sub-assembly build, cell and component QC and precise cell / stack assembly
- Further innovation in cell and seal manufacture, as well as greater automation such as high speed automated screen printing



Low Volume Raw Material Cost Comparison

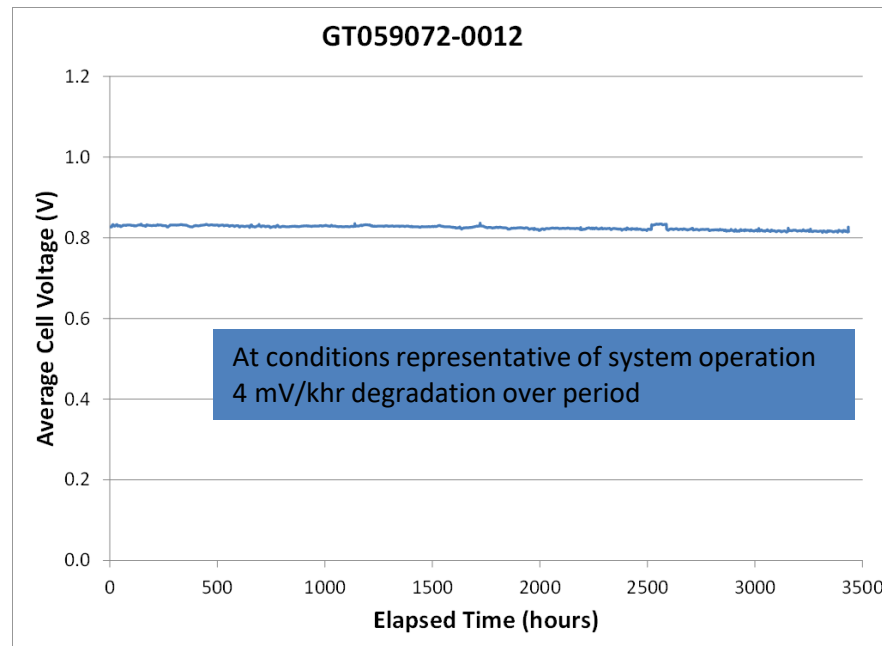
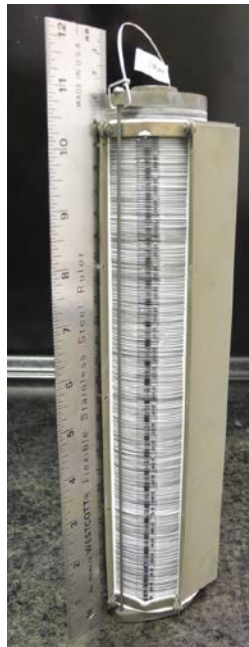
- Direct raw material content (steel, powders) of the baseline large area stack and CSA stack platform were compared from detailed bill of materials
- Basis:
 - Present day (0.3 MW/yr) material costs were selected
 - Stack performance on a per active area basis is identical

CSA Stack Material Cost Comparison



➤ Lightweight stack design translates directly to low amount (and cost) for input raw materials.

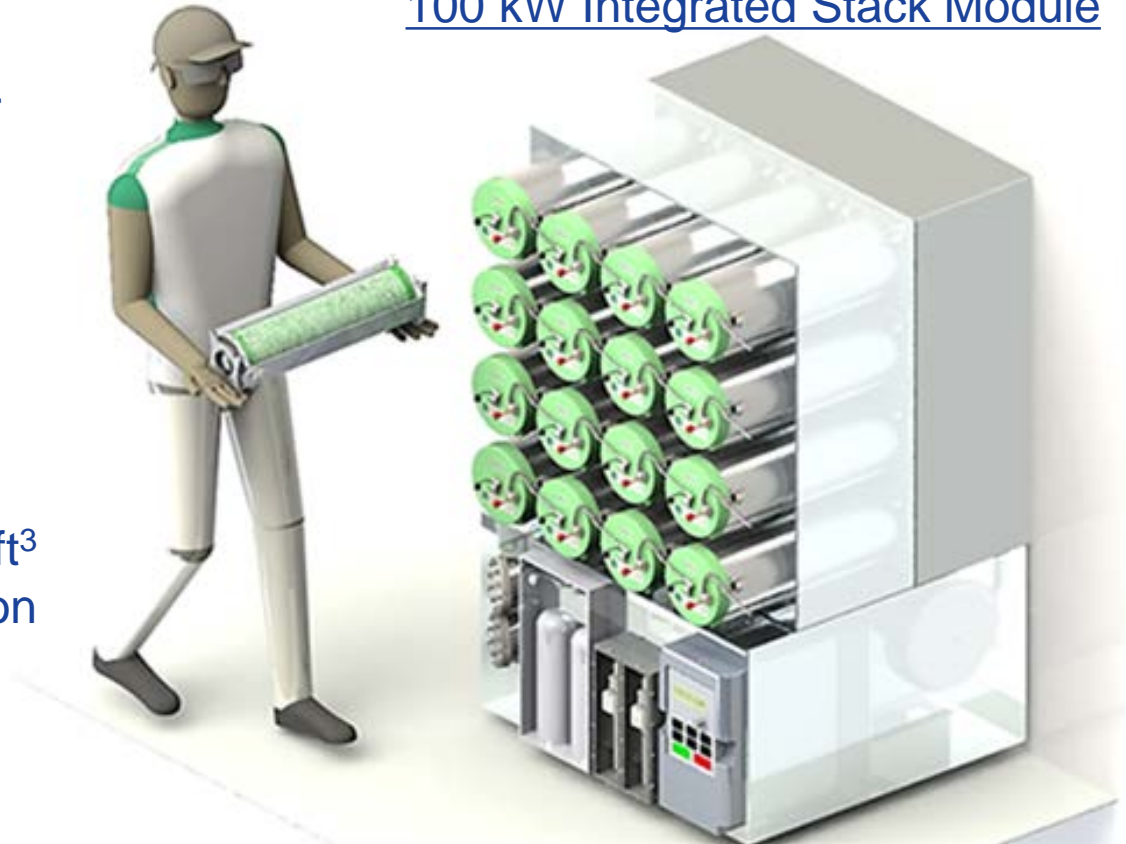
- Initial detailed design for CSA stack completed
- Majority of parts in-house or on order
- Robotic manufacturing work cell 80% complete
- Targeting first build trials and stack testing starting in Q3 this year
- Thin cell performance and degradation successfully demonstrated and looking positive for stack integration



CSA-like Sub-Scale Demonstration Stack
Test under System Gas fuel conditions

100 kW Integrated Stack Module

- Includes close-coupled hot-BoP components
- Serviceable by a single technician, minimal tooling
- High availability due to sparing philosophy
- Potential for significantly lower \$/kW and higher kW/ft³ due to process intensification and compact stack design benefits



(Inverter and Fuel Desulfurization not shown)

➤ Transformational stack enables low-cost and compact hot-module designs that are scalable for MW-class systems

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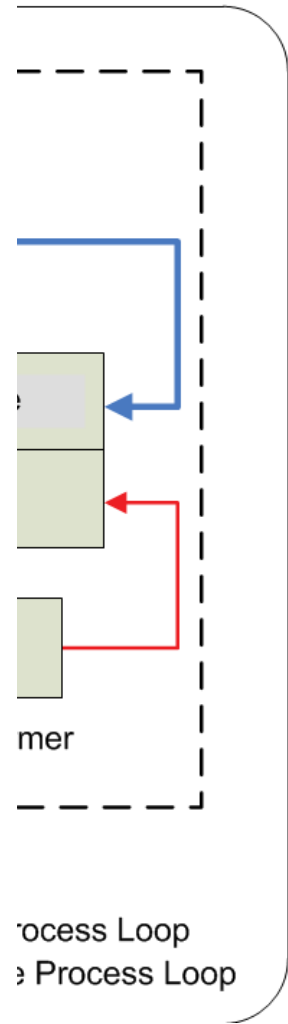
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200 kW SOFC System Performance Summary

SOFC Gross Power	Normal Operating Conditions		Rated Power	
DC Power	225.0	kW	244.0	kW
Energy & Water Input				
Natural Gas Fuel Flow	19.7	scfm	21.6	scfm
Fuel Energy (LHV)	323.2	kW	355.5	kW
Water Consumption @ Full Power	0	gpm	0	gpm
Consumed Power				
AC Power Consumption	10.8	kW	12.5	kW
Inverter Loss	11.3	kW	12.2	kW
Total Parasitic Power Consumption	22.0	kW	24.7	kW
Net Generation & Waste Heat Availability				
SOFC Plant Net AC Output	203.0	kW	219.3	kW
Available Heat for CHP (to 48.9°C)	84.7	kW	90.8	kW
Exhaust Temperature - nominal	370	°C	370	°C
Efficiency				
Electrical Efficiency (LHV)	62.8	%	61.7	%
Total CHP Efficiency (LHV) to 48.9°C	89.0	%	87.2	%

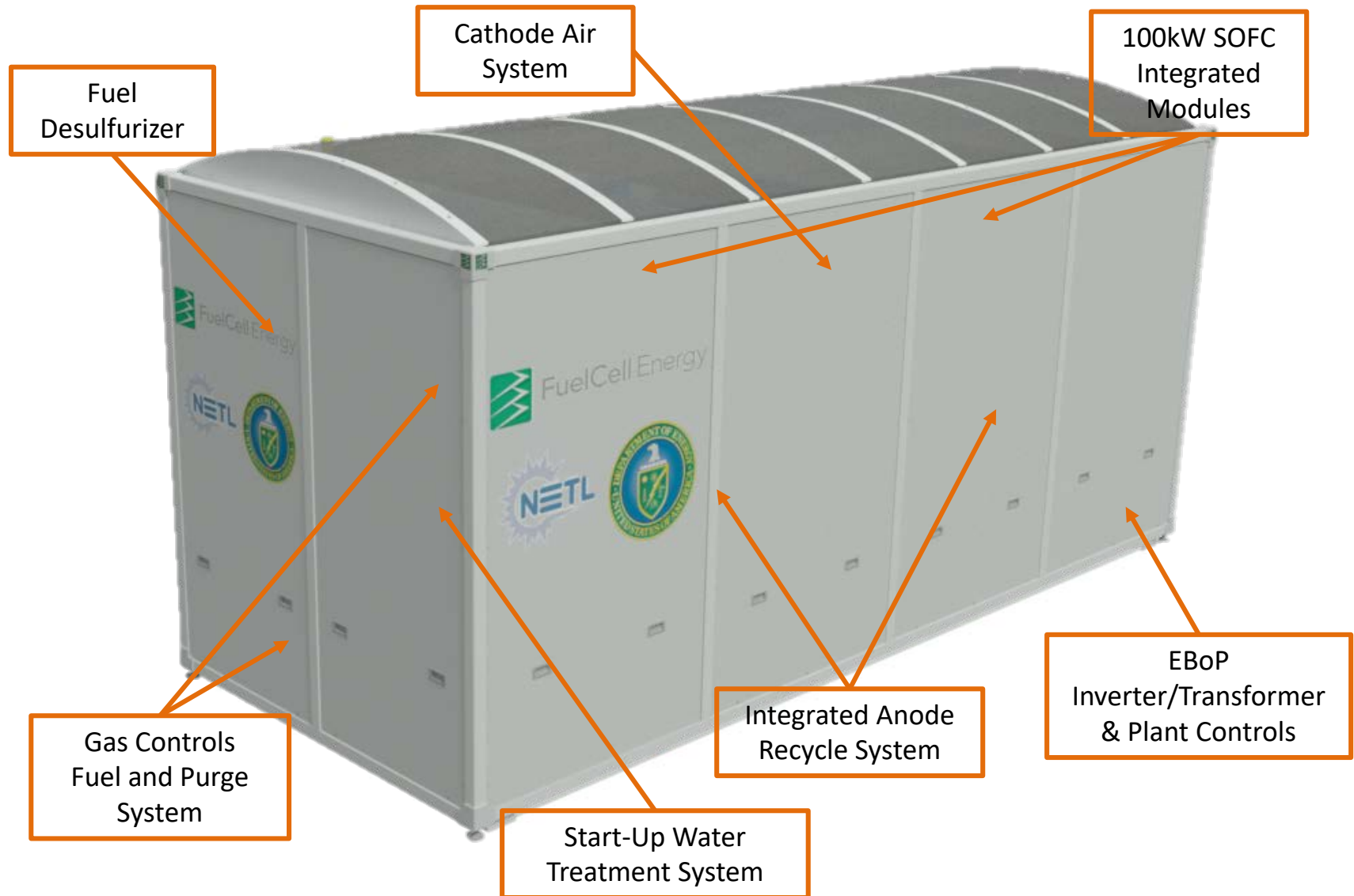
Air →
Moderate temperature to reduce cost increasing reliability

Fuel Gas → Des
Startup Water →

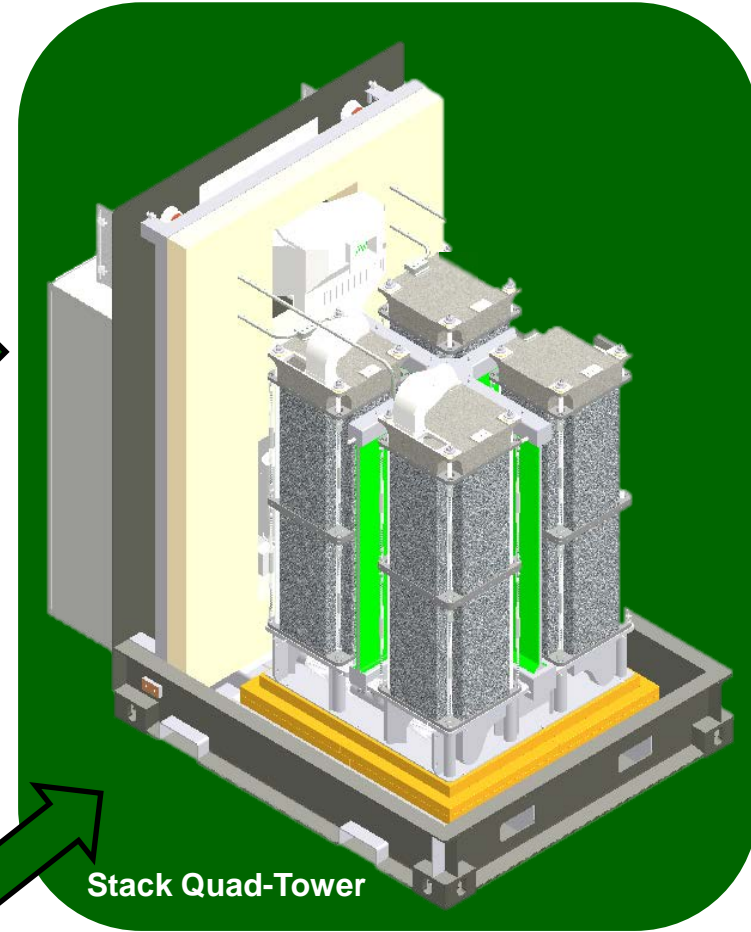
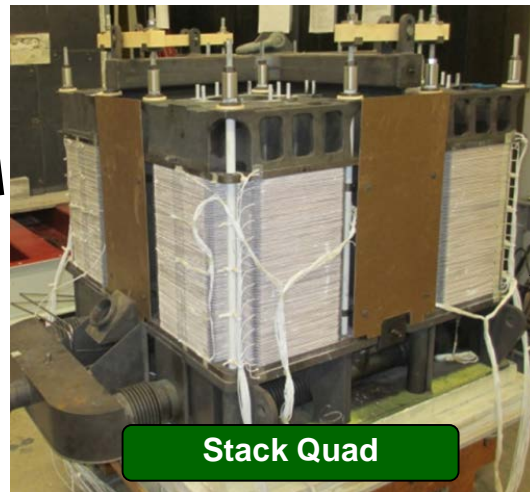
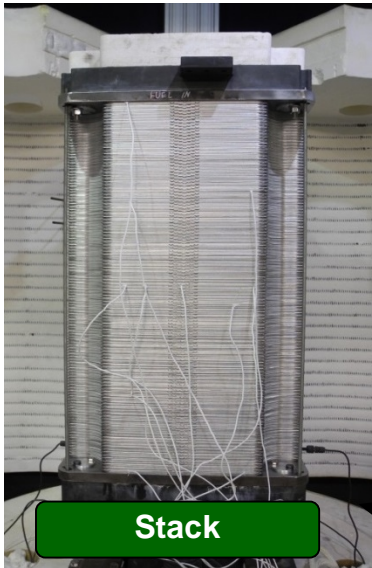


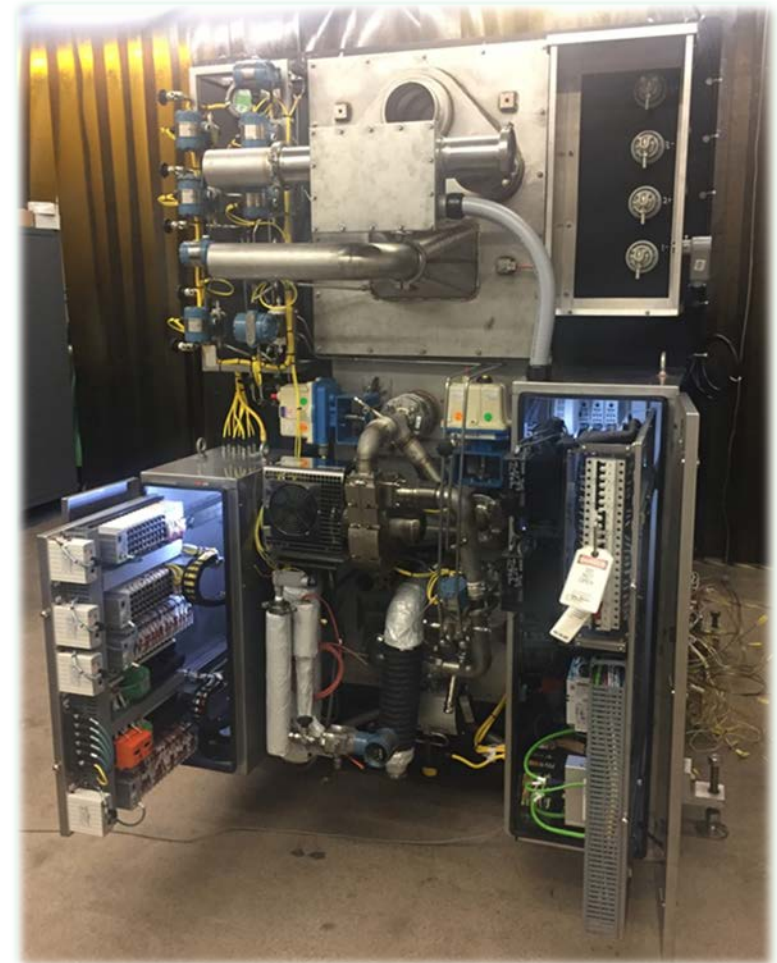
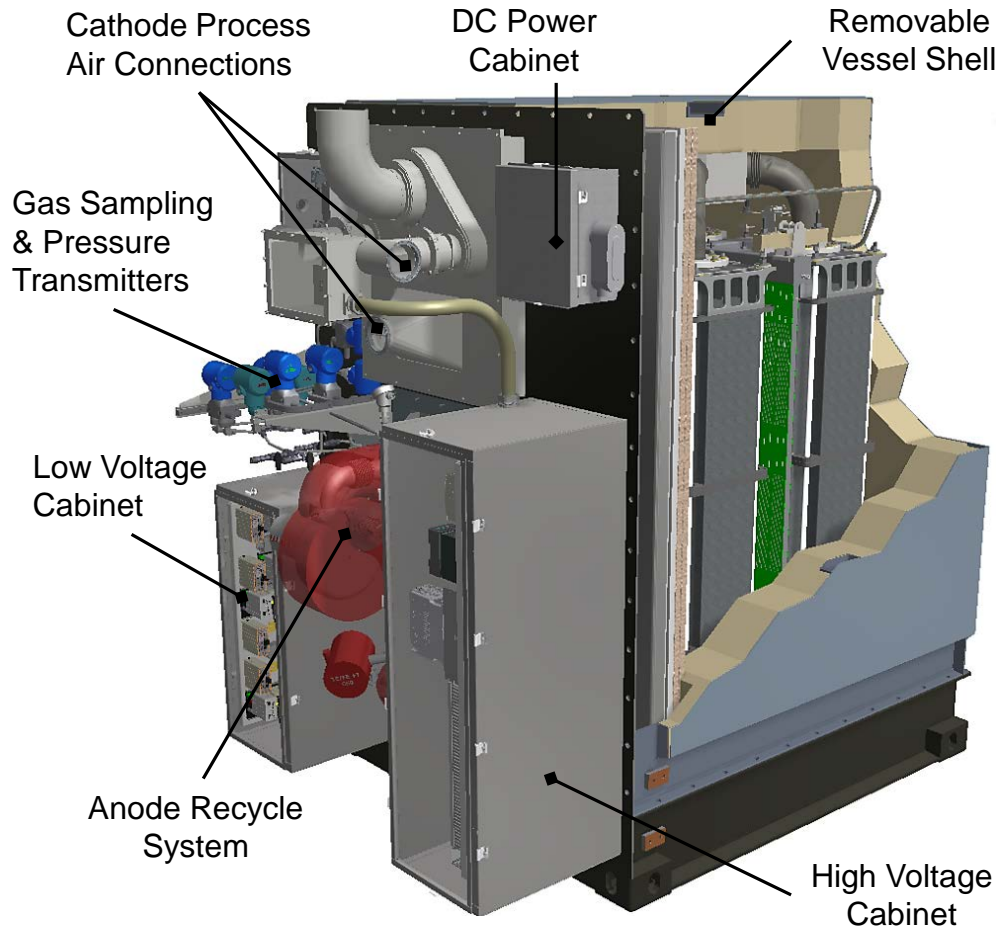
➔ 200 kW Modular Power Block (MPB) system is designed to validate stack reliability and scalable stack-module design.

200kW SOFC Power System Layout



- Includes (2) 100kW SOFC Module Power Blocks (MPB) designed to operate independently
- Factory assembled & shipped as a standard ISO 20' x 8' container



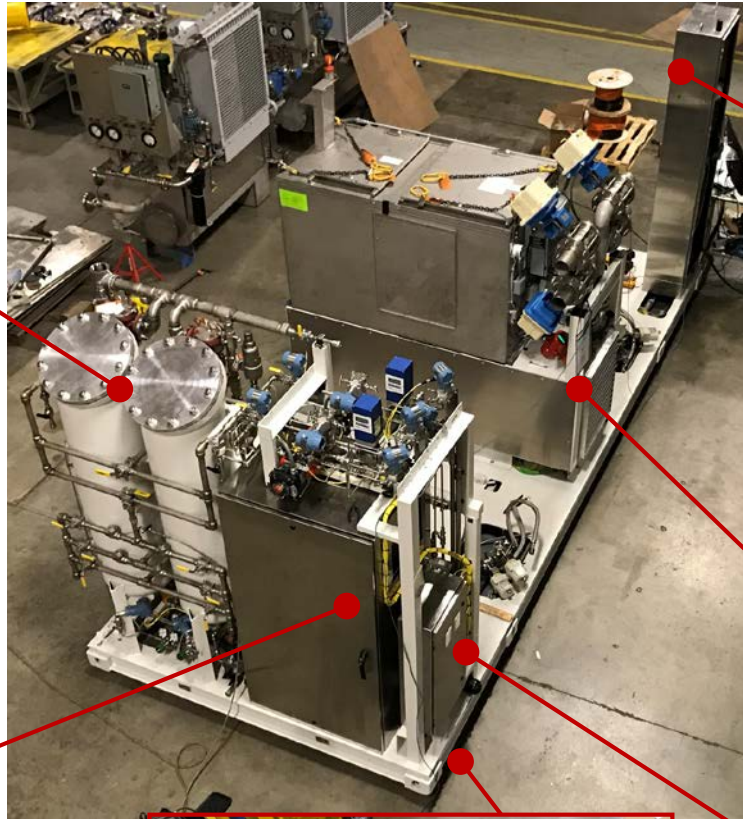


100 kW MPB Architecture:

- Fully integrates all hot BoP equipment within the module
- Eliminates high-temperature plant piping & valves
- Reduces Cr evaporation protective coatings within plant/module
- Integrated anode blower & module-specific instruments greatly decreases plant footprint



Desulfurization Units



Process Control System (PCS)



Air Delivery System



Start-up Water System



Skid Support-Integrated Piping

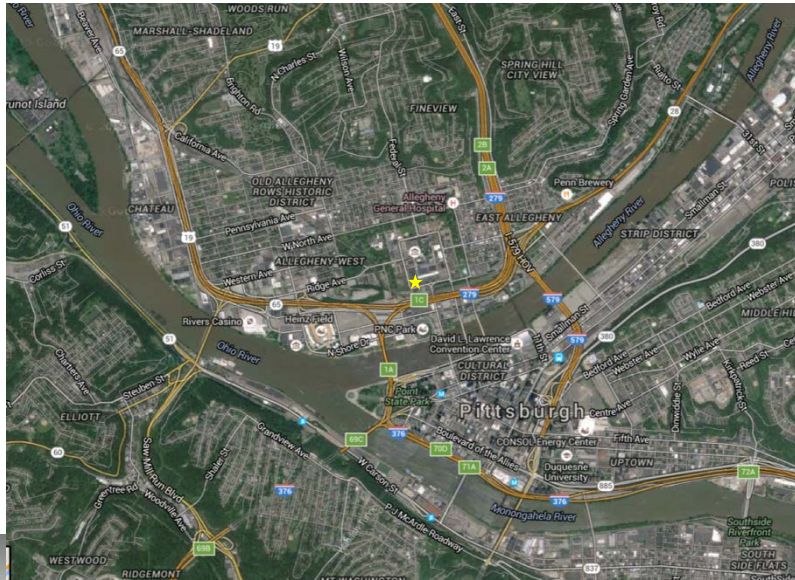


Remote I/O Cabinet (RIO)



1-Piece Ship & Install

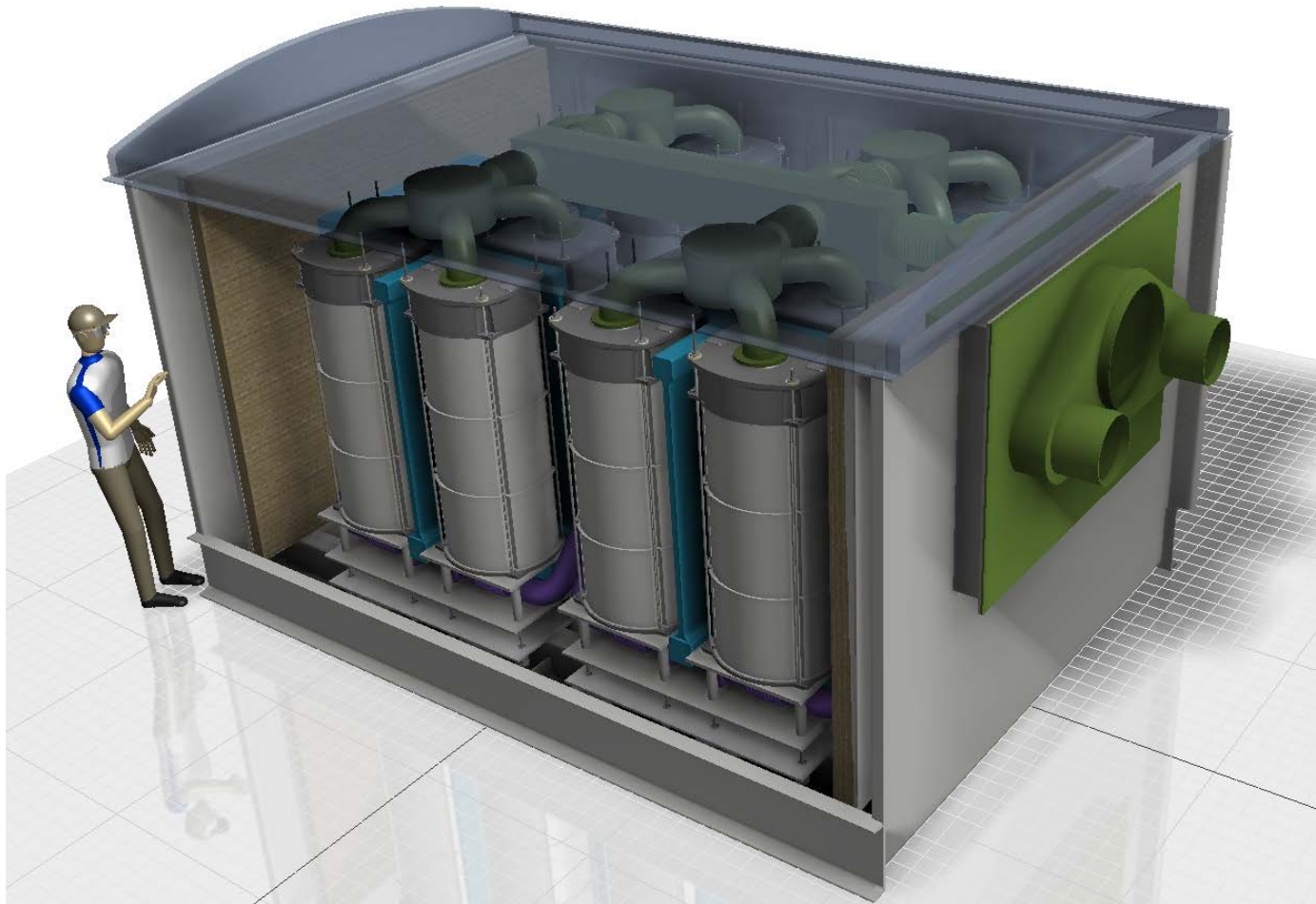
➔ 200 kW BoP (operating with 1 Module) installed at FCE's Danbury, CT Test Facility. BoP/Module validation testing is underway.



**NRG Energy Center
111 S Commons,
Pittsburgh, PA 15212**



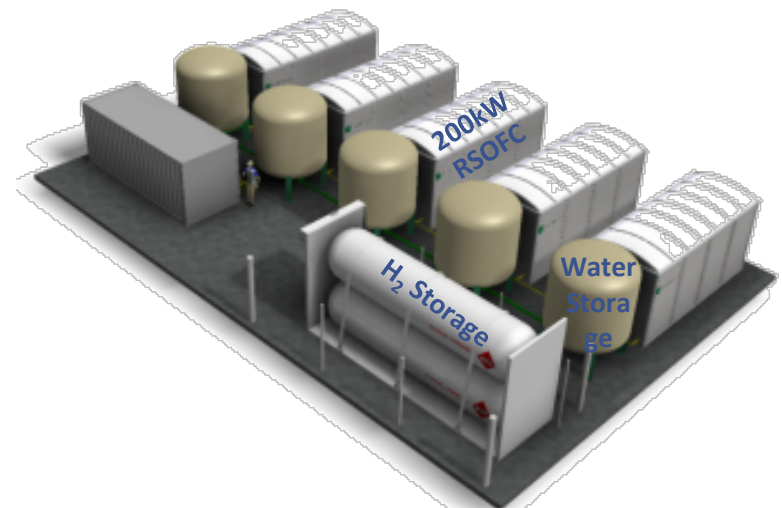
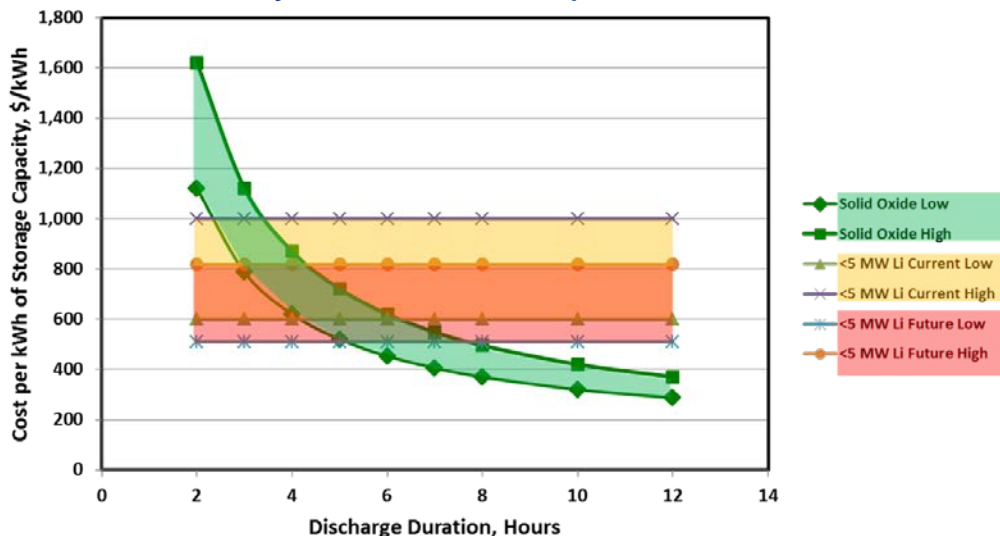
**System Installation
Planned Q3 – 4, 2017**




- MW-Class concept design utilizes proven quad-base SOFC stack tower configuration to minimize scale-up risk.
- Integrated hot-BoP components to minimize cost and footprint
- Module power density (0.7 kW/ft^3), nearly twice the value for 100 kW module ($.4 \text{ kW/ft}^3$) ³⁸

- In addition to the opportunities for low-cost power production, CSA-style stacks have been demonstrated in electrolysis (SOEC) and reversible (RSOFC) modes
- Advantage over conventional storage:
 - Long duration achieved by adding hydrogen storage, without adding stacks
- Advantage over other hydrogen-based storage:
 - Efficiency advantage – due to higher efficiency of SOFC in fuel cell and electrolysis modes of operation

**Baseline 20 cell
CSA-style stack:
Demonstrated
stable electrolysis
operation at 2
A/cm²**

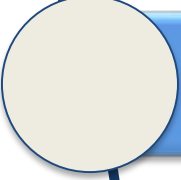


6 MWh RSOFC System
(1MW x 6 h)

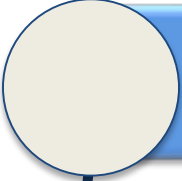
A light beige circular icon with a dark blue outline, connected to the text box by a dark blue line.

Incorporated Gen 2 Cr-mitigation technology into 80-cell stack demonstrating low degradation (0.4%/kh) in ongoing test

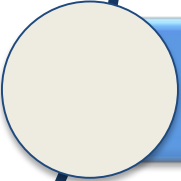
Gen 2 Cr-mitigation now being manufactured into 120-cell (16 kW) stacks for System Demo

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Developed cells with improved redox tolerance (94% lower loss after 6 redox cycles) to extend life in real-world system operating environment

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Improved SOFC manufacturing & enhanced Quality Control specifications, tools and procedures increasing stack reliability and endurance

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Developed and initiated fabrication of new Compact Stack Architecture (CSA) stack with potential significant reduction in raw material cost, and scalability for MW-class systems

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Completed fabrication and initiated testing of a highly integrated 100 kW Modular Power Block and 200 kW SOFC system balance of plant

Preparations for a 200 kW System Demo Field Test are underway

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Guidance from NETL Management team: Shailesh Vora, Joseph Stoffa, Patcharin Burke, and Heather Quedenfeld

